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(33) JP

(71) Applicants

Sumitomo Seika Chemicals Co. Ltd

(Incorporated in Japan)

346-1 Miyanishi, Harima-cho, Kako-gun, Hyogo, Japan

Suntory Limited

(Incorporated in Japan)

1-40 Dojimahama 2-chome, Kita-ku, Osaka-shi, Osaka,
Japan

(72) Inventors

Masakazu Takahashi

Johji Ogasahara

(51) INT CL⁵

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(56) Documents cited

GB 1575827 A

US 4511508 A

US 4282259 A

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INT CL⁵ C12C

Online database: WPI, CLAIMS, FOOD SCIENCE &
TECHNOLOGY ABSTRACTS

Miyoko Ono

Kazuhiro Hamatani

(74) Agent and/or Address for Service

Elkington and Fife

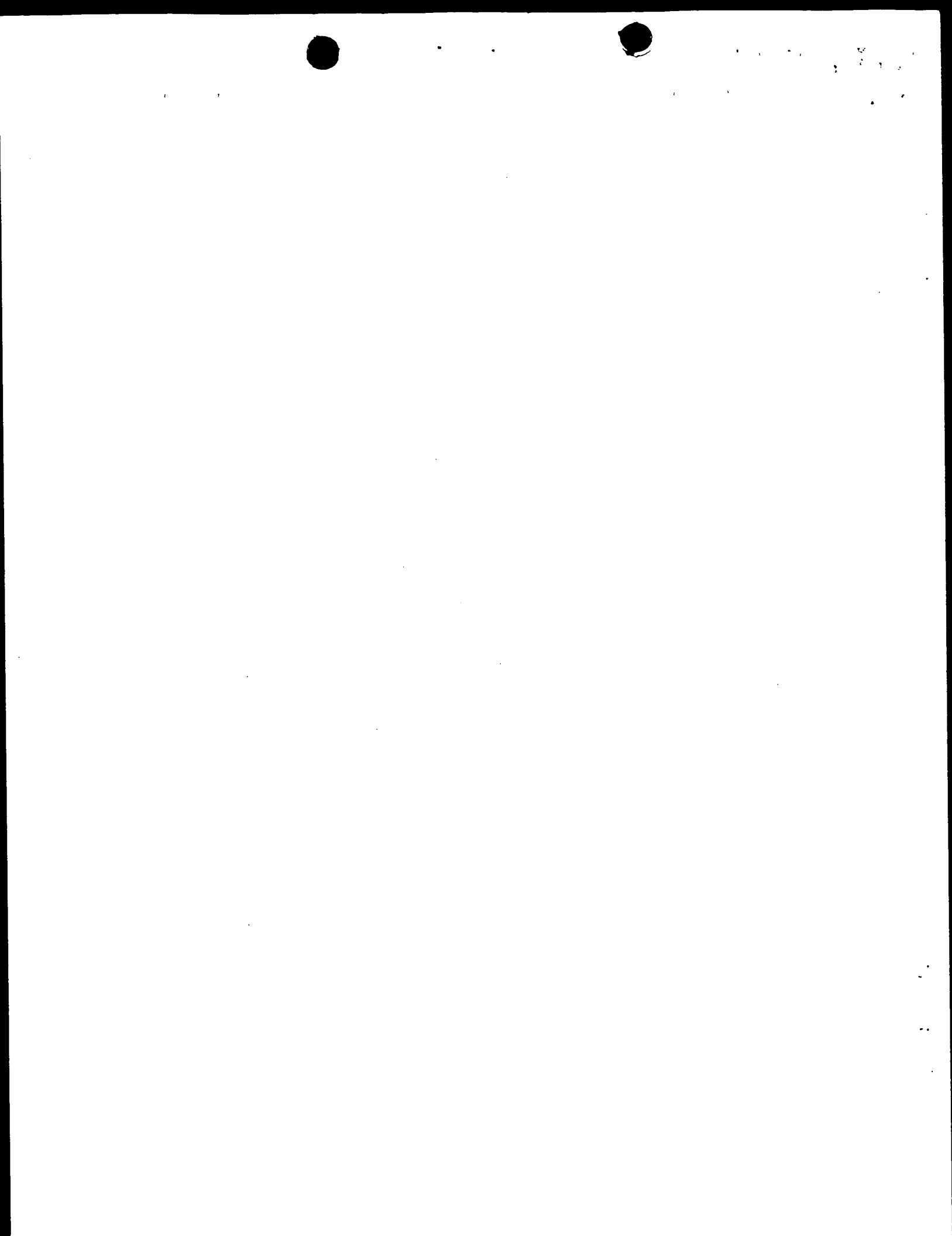
Prospect House, 8 Pembroke Road, Sevenoaks, Kent,
TN13 1XR, United Kingdom

(54) Extracting hops using dry recycled carbon dioxide

(57) A method for producing hop extracts containing small amounts of resin deterioration products, comprises extracting the hop extracts from dry hops using recycled carbon dioxide wherein said carbon dioxide is in a dry subcritical or supercritical condition.

The hop extracts thus obtained are useful in the production of high quality beer having a sharp and refreshing taste.

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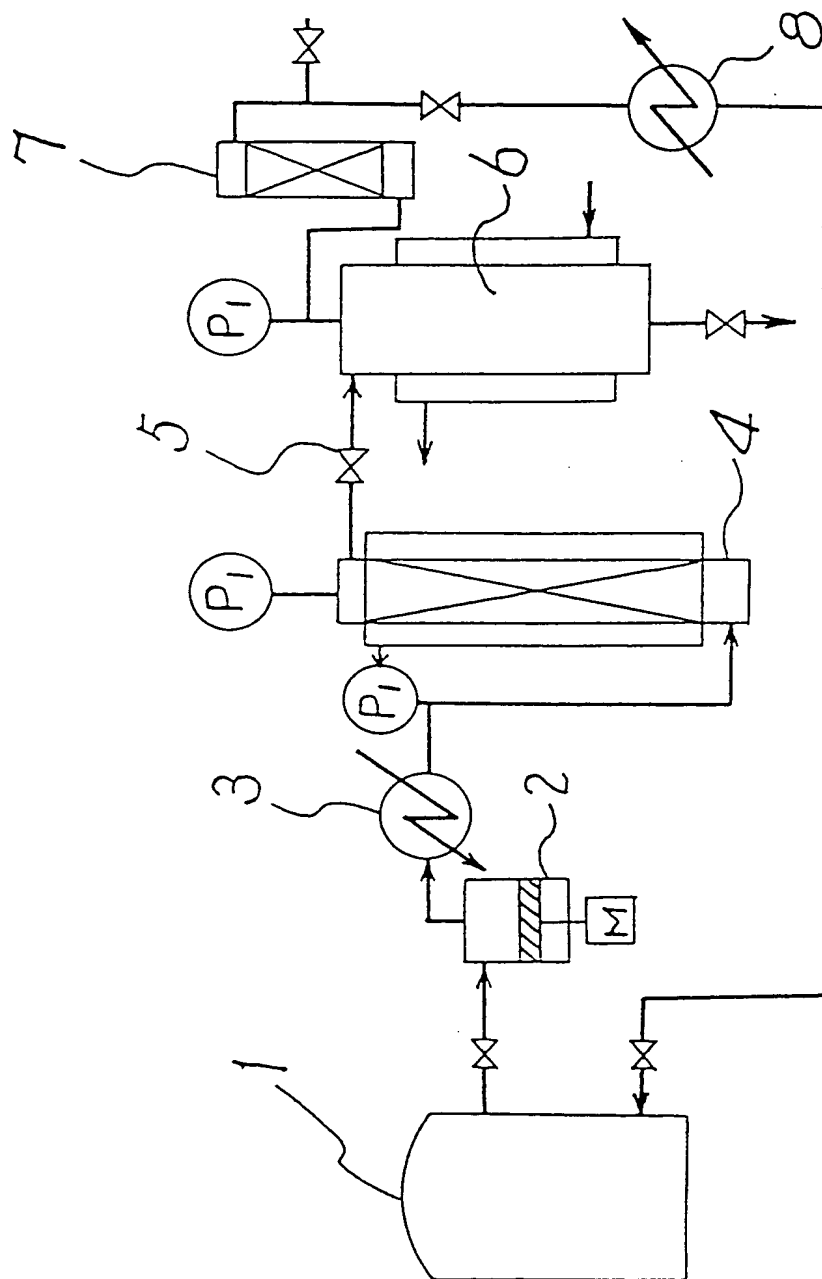


FIG. 1

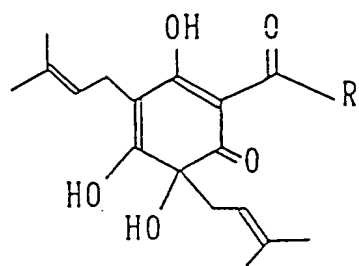
METHOD FOR PRODUCTION OF HOP EXTRACTS AND HOP EXTRACTS OBTAINED THEREBY

FIELD OF THE INVENTION

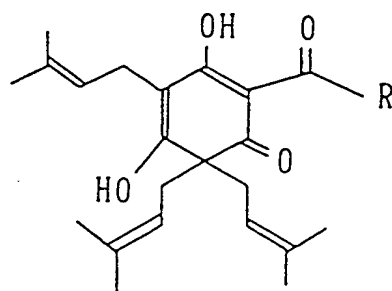
The present invention relates to a method for production of hop extracts, more specifically to a method for producing hop extracts which contain the reduced amounts of deteriorated resin products using dry carbon dioxide in a subcritical or supercritical condition as extracting agent, and to the hop extracts obtained thereby.

BACKGROUND OF THE INVENTION

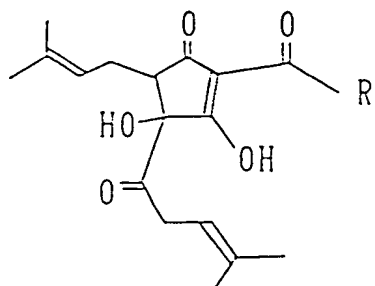
Hops, one of the major raw materials for beer, are used for giving a characteristic aroma and a refreshing bitter taste to beer. When hops are boiled along with the wort prior to the fermentation process, essential oils which provide the aroma and bitter taste components which provide the refreshing bitter taste are extracted and subsequently thermal isomerization takes place, whereby the wort comes to have the characteristic hop flavour. In the method described above, the bitter taste components, e.g., α -acids (Structural Formula 1), a major component of the soft resins of hops, isomerizes to water-soluble bitter taste components, mainly iso- α -acids (Structural Formula 3), during boiling the wort to give a refreshing sharp bitter taste to beer. As for β -acids (Structural Formula 2), another major component of the soft resins of hops, only a very small amount is extracted and transferred into the wort because its water-solubility is extremely low.



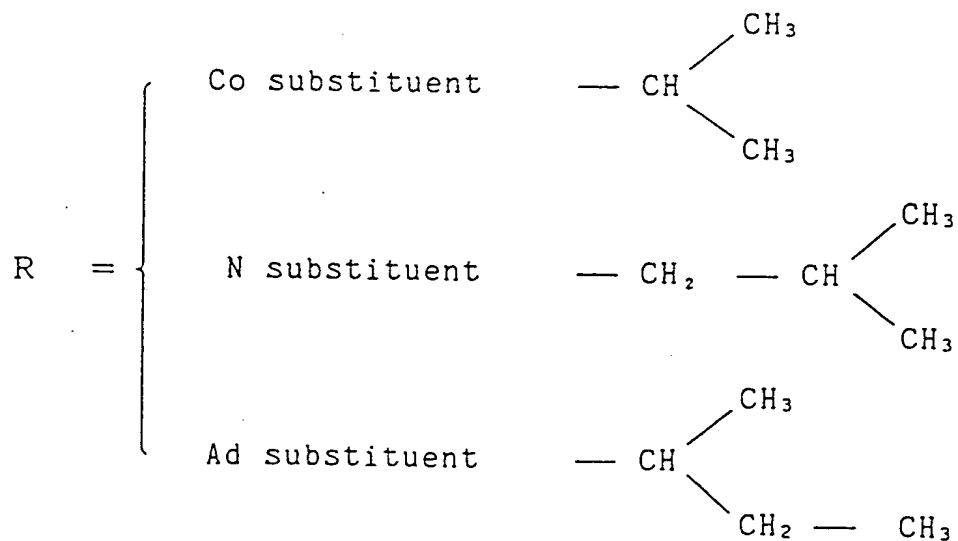
(1) α -acids



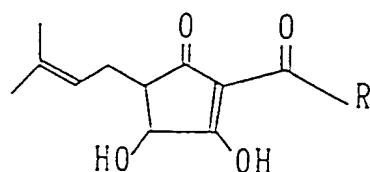
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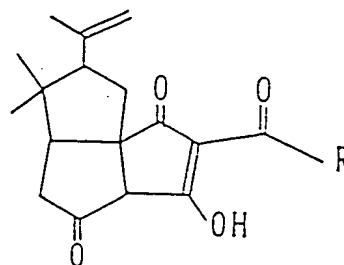
(3) iso- α -acids



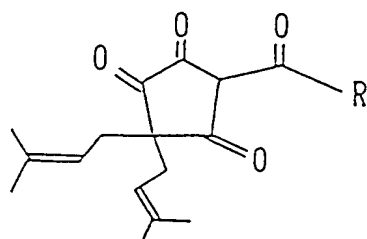
However, hops must be used after storage in the dried form after harvesting and in the form of whole hops, hop powder, hop pellets and so on, since it is difficult to harvest hops all through the year. Moreover, hops are very susceptible to oxidation; when α -acids or β -acids, major components of the soft resins of hops, are oxidized, the resulting deteriorated resin products such as humulinic acids (Structural Formula 4), tricyclodehydroisohumulones (Structural Formula 5) and hulupones (Structural Formula 6) are extracted and transfer into the wort and most of them transfer into beer because they are highly soluble in water.



(4) humulinic acids



(5) tricyclodehydroisohumulones



(6) hulupones

When these deteriorated resin products exist in beer, they deteriorate the quality of the beer. The degree of production of these deteriorated resin products depends on conditions of the hop drying stage, processing stage, storage and other factors. With respect to the production mechanism and the effects on the quality of beer, the present inventors have already investigated in detail (M. Ono, Y. Kakudo, R. Yamamoto, K. Nagami and J. Kumada, J. Amer. Soc. Brew. Chem., vol. 45, pp. 61-69, 1987).

As stated above, hops are susceptible to oxidation, and oxidized hops deteriorate the quality of beer; therefore, degassing and strict temperature control are necessary during the drying and processing stages. For storage, a warehouse equipped with large refrigerating equipment is necessary, which also requires strict control.

On the other hand, there is a method in which only desired components are extracted from hops with organic solvents and used as the hop extracts in place of hops themselves. In this case, the desired components are stored in the form of concentrated hop extracts; therefore, the hop extracts offer advantages of easy handling and storage space reduction. However, the hop extracts using organic solvents have various problems as follows.

1) Hard resin, tannin, fats, wax and pigments such as chlorophyll are extracted along with the desired components for beer flavour and the hop extracts have poor colour. Beer prepared using the extracts may lack refreshment and

excess miscellaneous tastes.

2) It is feared that harmful organic solvents may remain in the hop extracts.

3) Upon distilling off the organic solvent, the flavour components escape, and deteriorated resin products increase due to heating.

On the other hand, as a method of efficient extraction of desired components from natural products without the problem of residual organic solvent, supercritical fluid extraction using carbon dioxide (West German Patent Publication No. 2127618) is known. Examples of published application of this method applied to hops include Japanese Patent Examined Publication Nos. 44864/1973 and 41375/1989 and US Patent Nos. 4104409 and 4344978.

However, none of these attempts based on the prior art method aims at producing hop extracts containing the reduced amounts of deteriorated resin products; there is no disclosure other than a supercritical fluid extraction method using carbon dioxide and a production method for hop extracts having a low tannin content.

Based on the method described above, the present inventors attempted to use carbon dioxide in a subcritical or supercritical condition to produce hop extracts which contain the reduced amounts of deteriorated resin products.

It was found, however, that if carbon dioxide is recycled and reused after extraction and separation of hop extracts, the desired object cannot be accomplished because

of simultaneous extraction of a part of the deteriorated resin products. On the other hand, if carbon dioxide is not recycled but vented into the atmosphere after separation of hop extracts, the amount of simultaneously extracted deteriorated resin products can be reduced, but a huge amount of fresh carbon dioxide is necessary, which is too expensive for the production of hop extracts. In addition, ventilation carbon dioxide into the atmosphere involves a critical problem of escape of the desired flavour components characteristic to hops.

Although some other methods are available in which the desired components, e.g., soft resins and essential oils, are selectively separated under finely set separating conditions or in which the deteriorated resin products are selectively separated and removed, these methods are undesirable from the economic and operational viewpoints because the equipment is complex and process control is troublesome.

As stated above, by the prior art method, it is difficult to economically and efficiently produce hop extracts containing the large amounts of desired components and the reduced amounts of deteriorated resin products without a loss of flavour components.

SUMMARY OF THE INVENTION

It is an object of the present invention to provide a method for producing hop extracts which contain the reduced amounts of deteriorated resin products using dry carbon dioxide in a subcritical or supercritical condition as

extracting agent, and the hop extracts obtained thereby.

The inventors found that when extraction is conducted using carbon dioxide in a subcritical or supercritical condition, a correlation exists between the water content in carbon dioxide and the amount of deteriorated resin products extracted, and the water content affects the solubility of the deteriorated resin products in carbon dioxide.

In other words, with the recognition of the action of the water in carbon dioxide to increase the solubility of some deteriorated resin products in carbon dioxide, the inventors found that extraction of deteriorated resin products can be suppressed by reducing the water content in carbon dioxide and thus developed the present invention.

Here, the water in carbon dioxide is mostly the water which has transferred therein upon contact thereof with raw material hops, since carbon dioxide itself contains only a trace amount of water. Therefore, when hop extracts are extracted using recycled and reused carbon dioxide, almost all water in carbon dioxide originates from the water in hops.

Generally, hops are used as raw material hops, which contain 5 to 20% water. If the water content is to be reduced, the object can easily be accomplished by increasing the degree of dryness of the raw material hops. However, this approach is undesirable for some reasons, for example, drying above the normal degree of dryness is not only expensive but also leads to a loss of flavour components,

results in an increase in deteriorated resin products due to heating and causes a tendency toward absorption to hops during storage.

Therefore, for reducing the water content in carbon dioxide, it is simpler and more economic to use the method in which recycled and reused carbon dioxide is brought into contact with a desiccant and to remove the water therein which has transferred from the raw material hops.

The present invention was developed on the basis of these findings. Essentially, the invention relates to:

- (1) a method for producing hop extracts which contain the reduced amounts of deteriorated resin products by extracting from hops using recycled and reused carbon dioxide wherein said carbon dioxide is in a subcritical or supercritical condition, and
- (2) the hop extracts which contain the reduced amounts of deteriorated resin products obtained by the method for production described in (1) above.

BRIEF DESCRIPTION OF THE DRAWING

Figure 1 shows a flow sheet of a mode of embodiment of the present invention, wherein the numerical symbols 1 through 8 respectively denote a carbon dioxide holder (1), a compressor (2), a heat exchanger (3), an extraction chamber (4), a pressure-reducing valve (5), a separation chamber (6), a drying chamber (7), and a condenser (8).

DETAILED DESCRIPTION OF THE INVENTION

As stated above, the water content in hops is 5 to

20%; extracting hops using dry carbon dioxide result in extraction of water along with the extracts. In this case, the water content in carbon dioxide can be appropriately adjusted by varying extraction conditions such as the amount of carbon dioxide recycled and extraction temperature, and is normally 1000 to 5000 ppm.

Carbon dioxide after being used for the extraction and separation process is brought into contact with a desiccant to remove water therefrom after separating the hop extracts. Since the amount of deteriorated resin products extracted simultaneously with the hop extracts from hops decreases as the water content in carbon dioxide decreases, it is necessary to minimize the water content. In this case, high quality hop extracts containing substantially no deteriorated resin products or significantly reduced amounts of deteriorated resin products can be obtained by carrying out the extraction in a subcritical or supercritical condition of carbon dioxide having a water content of not more than 1000 ppm, preferably not more than 500 ppm after contact with the desiccant. When the water content exceeds 1000 ppm, no effect on reducing the amount of deteriorated resin products is obtained, and the results obtained are substantially the same as those obtained using recycled and reused carbon dioxide without contact with a desiccant.

Although varieties of hops can be used as a raw material for the present invention, including whole hops, hop powder,

pelletized hops and milling products thereof, all dried by an ordinary drying method, it is advantageous from the viewpoint of extraction efficiency to use hops in a milled form.

However, since not only the form of hops but also the variety, quality and other features of raw material hops significantly affect the quality of the obtained hop extracts and in turn the quality of beer, the raw material hops must be selected according to the purpose in advance.

The subcritical or supercritical carbon dioxide used as extracting agent in the present invention is non-flammable, harmless, cheap, and easy to handle with a critical temperature of 31.3 °C and a critical pressure of 72.9 atm. In addition, a supercritical fluid has a density close to that of liquid and a high value of diffusion coefficient close to that of gas, which characteristics give the supercritical fluid the capability of quickly extracting large amounts of various compounds with high yield. Moreover, supercritical carbon dioxide is easy to be separated from the extracts by slightly changing the pressure or temperature, and even offers a bacteriostatic or bactericidal effect, as advantage characteristic to carbon dioxide. It is thus harmless to humans and sanitary. For these reasons, it is especially suitable for use in foods and pharmaceuticals, and is preferably used to obtain hop extracts, the desired product of the present invention.

When dry subcritical or supercritical carbon dioxide is

used as extracting agent, the carbon dioxide pressure and temperature in the extraction chamber must be kept normally at 60 to 400 kg/cm², preferably at 100 to 350 kg/cm² and normally at 25 to 100°C, preferably at 30 to 70°C, respectively, during extraction. This is because pressures and temperatures exceeding the respective upper limits result in increased equipment cost, which is undesirable from the economic viewpoint, and pressures and temperatures below the respective lower limits hamper efficient extraction of hop extracts.

As for separating conditions in the separation chamber, good results are obtained when the pressure and temperature are kept at 20 to 150 kg/cm², preferably 30 to 100 kg/cm², and 25 to 100°C, preferably 30 to 70°C, respectively. It is also possible to selectively obtain a particular component free of deteriorated resin products by varying separating conditions such as separation pressure and separation temperature on a time basis or by carrying out separation in a number of stages.

It is preferable that contact of desiccant and carbon dioxide is achieved by flowing carbon dioxide through a desiccant-packed chamber prior to re-introducing carbon dioxide into the extraction chamber after separating the hop extracts because this method is efficient and has little influence on the hop extracts.

In the present invention, various commonly known desiccants can be used. Examples of such desiccants include

silica gel, calcium chloride, calcium sulfate, magnesium oxide, aluminum oxide, water-absorbing resins (e.g., Aquakeep, produced by Sumitomo Seika Chemicals Co., Ltd.) and porous materials (e.g., molecular sieves), with preference given to silica gel, calcium chloride, molecular sieves, etc. because they are easily available, economic and desirable from the viewpoint of food hygiene.

When hops are extracted by the method of the present invention, the obtained hop extracts which contain the reduced amounts of deteriorated resin products. Here, "the reduced amounts of deteriorated resin products" includes the case where substantially no deteriorated resin product is contained. When ordinary hops are used as a raw material, the obtained effect is such that substantially no deteriorated resin products is contained, as described in Examples below. Also, even when using deteriorated hop pellets containing intentionally increased amount of deteriorated resin products, the amount of deteriorated resin products extracted along with the hop extracts is very small.

A mode of embodiment of the present invention in which dry carbon dioxide in a subcritical or supercritical condition is used as extracting agent is hereinafter described by means of the flow sheet shown in Figure 1.

Figure 1 illustrates a case where a drying chamber 7 is arranged after a separation chamber 6.

In Figure 1, carbon dioxide, compressed to a given pressure by means of a compressor 2, is passed from a carbon

dioxide holder 1 through a heat exchanger 3 to heat to a given extraction temperature and then introduced into an extraction chamber 4 while maintaining a subcritical or supercritical condition. The extraction chamber 4 has been charged with raw material hops.

After extraction with the subcritical or supercritical carbon dioxide, the extract-containing carbon dioxide is passed through a pressure-reducing valve 5 to reduce its pressure and then introduced into a separation chamber 6, where the extracts are separated from the carbon dioxide. After separating the extracts, the carbon dioxide is introduced into a drying chamber 7, where the water in the carbon dioxide is removed by the charged desiccant. The carbon dioxide thus dried is cooled and liquefied in a condenser 8 and recycled via a compressor 2. In this manner, the subcritical or supercritical carbon dioxide as extracting agent is dried to remove water to not more than 1000 ppm and then recycled as dry carbon dioxide.

A method of the present invention characterized as above offers the following excellent effects.

(1) In the extraction of hop using subcritical or supercritical dry carbon dioxide as extracting agent, it is possible to produce high quality hop extracts which contain the reduced amounts of deteriorated resin products, (deteriorated resin products significantly affect the quality of beer) only by using dry carbon dioxide from which water has been removed by contact thereof with a

desiccant.

(2) The use of carbon dioxide as extracting agent makes it possible to obtain safe and sanitary hop extracts free of residual organic solvent.

(3) The recycling and reuse of carbon dioxide permits obtainment of hop extracts maintaining the rich hop flavour at low cost.

The hop extracts thus obtained, which contain the reduced amounts of deteriorated resin products, is very useful in the production of high quality beer having a sharp and refreshing taste and flavour.

EXAMPLES

The present invention is hereinafter described in more detail by means of the following working examples, comparative examples and test example, but the invention is never limited by these examples.

Example 1

Using the extraction chamber 4 having an inside capacity of 2ℓ illustrated in Figure 1, hops were extracted.

Specifically, 702 g of milled hop pellets (containing about 10% water), which are commonly used for producing beer, was charged in the extraction chamber and subjected to extraction and separation of hop extracts using supercritical carbon dioxide at an extraction chamber pressure of 230 kg/cm², an extraction chamber temperature of 40°C, a separation chamber pressure of 50 kg/cm² and a separation

chamber temperature of 40°C. The carbon dioxide which exited the separation chamber was passed through the drying chamber packed with 500 g of silica gel to thereby remove water, after which it was recycled.

After passage through the drying chamber, the carbon dioxide had a water content of 150 ppm.

After circulating carbon dioxide for about 5 hours, 102.8 g of light green hop extracts were obtained in the separation chamber. The residual hop pellets weighed 569.2 g.

The starting hop pellets and the hop extracts obtained were analyzed for major components and deteriorated resin products by liquid chromatography. The results are shown in Table 1.

The analysis by liquid chromatography was conducted by the method of Ono et al. (M. Ono, Y. Kakudo, R. Yamamoto, K. Nagami and J. Kumada, J. Amer. Soc. Brew. Chem., vol. 45, pp. 70-76, 1987). The unit amount of deteriorated resin products is expressed as the ratio of the peak area from the group of deteriorated resin products to the peak area from the internal standard substance.

No deteriorated resin product was detected in the hop extracts obtained.

In the production of beer, α -acids in hops isomerize to iso- α -acids during boiling of the wort to give a refreshing bitter taste to beer as stated above; therefore, the amount of hops used is determined from the α -acids content in the

hops in most cases. Since almost all deteriorated resin products in hops transfer into beer, the amount of deteriorated resin products produced per gram of α -acids was calculated. The results are also shown in Table 1. The bitter taste quality of beer improves as this amount of deteriorated resin products produced per gram of α -acids decreases.

Example 2

Hops were extracted and separated under the same conditions as in Example 1 except that the amount of milled hop pellets was 669 g and the drying chamber was packed with 500 g of calcium chloride in place of silica gel. After passage through the drying chamber, the carbon dioxide had a water content of 278 ppm.

After circulating carbon dioxide for about 5 hours, 93.7 g of light green hop extracts were obtained in the separation chamber. The residual hop pellets weighed 532.6 g.

The starting hop pellets used and the hop extracts obtained were analyzed by liquid chromatography in the same manner as in Example 1. The results are shown in Table 1. No deteriorated resin product was detected in the hop extracts.

Example 3

Using supercritical carbon dioxide, hops were extracted and separated from 680 g of milled hop pellets in the same manner as in Example 1 except that the extraction chamber pressure was 150 kg/cm², the extraction chamber temperature was 50°C, the separation chamber pressure was 45 kg/cm²

and the separation chamber temperature was 40°C. The carbon dioxide which exited the separation chamber was passed through the drying chamber packed with 500 g of silica gel to thereby remove water, after which it was recycled.

After passage through the drying chamber, the carbon dioxide had a water content of 125 ppm. After circulating carbon dioxide for about 5 hours, 85.2 g of light green hop extracts were obtained in the separation chamber. The residual hop pellets weighed 559.8 g. The starting hop pellets and the hop extracts obtained were analyzed by liquid chromatography in the same manner as in Example 1. The results are shown in Table 1. No deteriorated resin product was detected in the hop extracts.

Example 4

Hops were extracted and separated under the same conditions as in Example 1 except that the amount of silica gel packed in the drying chamber was changed to 250 g. The recycled carbon dioxide had a water content of 450 ppm. 82.9 g of light green hop extracts were obtained in the separation chamber. The residual hop pellets weighed 521.7 g. The starting hop pellets and the hop extracts obtained were analyzed by liquid chromatography. The results are shown in Table 1. No deteriorated resin product was detected in the hop extracts obtained.

Example 5

Hops were extracted and separated under the same

conditions as in Example 2 except that the amount of calcium chloride packed in the drying chamber was changed to 200 g. The recycled carbon dioxide had a water content of 780 ppm. 84.0 g of light green hop extracts were obtained in the separation chamber. The residual hop pellets weighed 540.3 g. The starting hop pellets and the hop extracts obtained were analyzed by liquid chromatography. The results are shown in Table 1. As a result, only 0.36% of the deteriorated resin products present in the starting hop pellets were extracted along with the hop extracts.

Comparative Example 1

Hops were extracted and separated under the same conditions as in Example 1 except that the amount of milled hop pellets was 683 g and nothing was packed in the drying chamber. The recycled carbon dioxide had a water content of 1250 ppm. After circulating carbon dioxide for about 5 hours, 88.3 g of light green hop extracts were obtained in the separation chamber. The residual hop pellets weighed 580.3 g.

The starting hop pellets and the hop extracts obtained were analyzed by liquid chromatography in the same manner as in Example 1. The results are shown in Table 1. 36.9% of the deteriorated resin products present in the starting hop pellets was extracted along with the hop extracts.

Example 6

About 1 kg of the same hop pellets as used in Example 1 were kept standing in thermostat at 50°C for 18 hours to

increase amount of deteriorated resin products in the hop pellets (hereinafter referred to as deteriorated hop pellets). Hops were extracted and separated under the same conditions as in Example 1 except that 403 g of a milling product of the deteriorated hop pellets thus prepared was charged in the extraction chamber and supercritical carbon dioxide was circulated for 2 hours.

The carbon dioxide which exited the separation chamber was passed through the drying chamber packed with 500 g of silica gel to thereby remove water, after which it was recycled. After passage through the drying chamber, the carbon dioxide had a water content of 165 ppm.

After circulating carbon dioxide for about 2 hours, 21.3 g of light green hop extracts were obtained in the separation chamber. The residual hop pellets weighed 352.7 g.

The starting deteriorated hop pellets and the hop extracts obtained were analyzed by liquid chromatography in the same manner as in Example 1. The results are shown in Table 1. Only 3.7% of the deteriorated resin products present in the deteriorated hop pellets was extracted along with the hop extracts.

Comparative Example 2

Using supercritical carbon dioxide, hops were extracted and separated under the same conditions as in Example 6 except that 398 g of the same milled hop pellets as in Example 6 was charged in the extraction chamber, and nothing

was packed in the drying chamber. The recycled carbon dioxide had a water content of 1650 ppm.

After circulating carbon dioxide for about 2 hours, 20.8 g of light green hop extracts were obtained in the separation chamber. The residual hop pellets weighed 363.7 g.

The starting deteriorated hop pellets and the hop extracts obtained were analyzed by liquid chromatography in the same manner as in Example 1. As shown in Table 1, 43.1% of the deteriorated resin products present in the deteriorated hop pellets was extracted.

TABLE 1 (1)

No	Major components in hops					Major components in hop extracts				
	Total weight (g)	α -acids (g)	β -acids (g)	Resin deterioration (unit)	Resin deterioration per α -acids (unit)	Total weight (g)	α -acids (g)	β -acids (g)	Resin deterioration (unit)	Resin deterioration per α -acids (unit)
Ex 1	702	38.9	39.5	3.70×10^6	9.5×10^4	102.8	38.7	39.4	ND	—
Ex 2	669	37.1	37.7	3.53×10^6	9.5×10^4	93.7	37.0	37.7	ND	—
Ex 3	680	37.7	38.3	3.58×10^6	9.5×10^4	85.2	37.5	38.2	ND	—
Ex 4	633	35.1	35.6	3.34×10^6	9.5×10^4	82.9	35.0	35.5	ND	—
Ex 5	656	36.3	36.9	3.46×10^6	9.5×10^4	84.0	36.1	36.7	1.23×10^4	3.4×10^2
Ex 6	403	6.1	5.8	2.93×10^6	48.0×10^4	21.3	6.1	5.8	1.08×10^5	1.8×10^4
Com. 1	683	37.8	38.5	3.60×10^6	9.5×10^4	88.3	37.8	38.5	1.33×10^6	3.5×10^4
Ex 2	398	6.0	5.7	2.90×10^6	48.3×10^4	20.8	6.0	5.7	1.25×10^6	20.8×10^4

ND: No Detection

TABLE 1 (2)

No	Yields of each component		
	α - acids (%)	β - acids (%)	Resin deteriora- tion (%)
Ex 1	99.5	99.7	—
Ex 2	99.7	100	—
Ex 3	99.5	99.7	—
Ex 4	99.7	99.7	—
Ex 5	99.4	99.5	0.36
Ex 6	100	100	3.7
Com. 1	100	100	36.9
Ex 2	100	100	43.1

Test Example

The hop extracts obtained in Examples 4 and 6 and Comparative Examples 1 and 2 were used to produce beer. The beer thus obtained were subjected to sensory evaluation by six well trained panels with respect to oxidized hop odor, intensity of bitter taste, sharpness of bitter taste, refreshment and personal favor. The results are shown in Table 2. The amount of hop extracts used for beer was adjusted so that the beer products had the same bitter taste value.

T A B L E 2

Sensory evaluation	Example		Comparative Example	
	4	6	1	2
Oxidized hop odor	nothing	nothing	slightly	strong
Intensity of bitter	moderate	moderate	moderate	weak
Sharpness of bitter	good	good	a bit bad	bad
Refreshment	good	good	good	bad
Personal favor (favor/unfavor)	4 / 2	6 / 0	2 / 4	0 / 6

What is claimed is:

1. A method for producing hop extracts which contain reduced amounts of deteriorated resin products, comprising extracting with carbon dioxide which is recycled and reused in a subcritical or supercritical condition, wherein said carbon dioxide is dry.
2. A method according to claim 1, wherein the water content in said carbon dioxide is not more than 1000ppm.
3. A method according to claim 1, wherein said carbon dioxide in a subcritical or supercritical condition is in the range of a pressure of 60 to 400 kg/cm² and a temperature of 25 to 100°C.
4. A method according to claim 1, wherein said carbon dioxide is obtained by contact with desiccant prior to re-introducing into the extraction process after separating hop extracts.
5. A method according to claim 4, wherein said desiccant is selected from the group consisting of silica gel, calcium chloride, calcium sulfate, magnesium oxide, aluminum oxide, water-absorbing resin and porous material.
6. The hop extracts which contain the reduced amounts of deteriorated resin products, obtainable by the method of any one of claims 1 to 5.
7. A method according to claim 1, substantially as hereinbefore described with reference to any of the Examples and/or the accompanying drawing.

25
Patents Act 1977

Examiner's report to the Comptroller under
Section 17 (The Search Report)

Application number

9123216.5

Relevant Technical fields

(i) UK CI (Edition K) C6E (EHAA)

(ii) Int CI (Edition 5) C12C

Search Examiner

S E CHALMERS

Databases (see over)

(i) UK Patent Office

(ii) ONLINE DATABASES: WPI, CLAIMS, FODD SCIENCE
AND TECHNOLOGY ABSTRACTS

Date of Search

9.12.91

Documents considered relevant following a search in respect of claims

1-7

Category (see over)	Identity of document and relevant passages	Relevant to claim(s)
A	GB 1575827 (BREWING PATENTS) see eg figure 3	
A	US 4511508 (SKW TROSTBERG) see eg Examples 2 and 4	
A	US 4282259 (DISTILLERS) see eg the figures	

Category	Identity of document and relevant passages	Relevant to claim(s)

Categories of documents

X: Document indicating lack of novelty or of inventive step.

Y: Document indicating lack of inventive step if combined with one or more other documents of the same category.

A: Document indicating technological background and/or state of the art.

P: Document published on or after the declared priority date but before the filing date of the present application.

E: Patent document published on or after, but with priority date earlier than, the filing date of the present application.

&: Member of the same patent family, corresponding document.

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